## MARKED UP VERSION OF AMENDED CLAIMS

2. (Amended) The process [Process according to] of claim 1, [wherein] in which the temperature in the dense phase stripping zone is between about 500°C and about 600°C.

3. (Amended) The process [Process according to any one] of claim[s] 1[-2], [wherein] in which the weight ratio of spent catalyst obtained in step (b) which is sent to step (c) and of spent catalyst obtained in step (b) which is used in step (d) is between about 1:10 and about 10:1

4. (Amended) The process [Process according to any one] of claim[s] 1[-3], [wherein] in which the weight ratio of spent catalyst and regenerated catalyst in step (d) is between about 1:10 and about 10:1.

5. (Amended) The process [Process according to any one] of claim[s] 1[-4], [wherein] in which the separation of step (g) is performed in the gas-solid separation steps of step (a).

8. (Amended) The use [Use] of the unit as described in [any one of] claim 6[-7] for a process as described in [any one of] claim[s] 1 [to 5].

9. (Amended) The use [Use] of the unit as described in claim 7 for a process as described in [any one of] claim[s] 1[-5] in alteration with a use of the unit for a process in which the dilute phase stripping zone (B) is used as an additional reaction zone wherein to one reaction zone a mixture of steam and a hydrocarbon feedstock boiling below about 300 °C is supplied to.